1. Introduction

Fossil fuels is ourare the world's primary source of energy, in the world with accounting for more than 80 % of global energy consumption. Overconsumption of this non-renewable energy could contributes to global warming due to the massive emissions of greenhouse gases. The problems related to fossil fuels and the serious environmental concerns have motivated e people forts towards sustainability and enhanced engagement in green technology.

Biomass is considered one of the key solutions for <u>our</u> alternative energy <u>courceneeds</u>. Roughly <u>approximately about</u> 90% of biomass is disposed <u>of</u> as wastes in the palm oil <u>industrymill</u>². In addition, 351 palm oil mills in <u>mMalaysia</u> produced 30 million tonnes of empty fruit bunches (EFB) from 83 million dry tonnes of solid biomass in 2012. The abundance of <u>underutilised</u> biomass feedstock which are underutilised has gained growing interest among researchers as a potential solidfuel energy resource.

However, biomass feedstock cannot be directly <u>feadimplemented</u> into the existing combustion system due to <u>its</u>-unfavourable properties, such as low calorific value, high moisture content and reduction in quality via biodegradation. <u>The bB</u>iomass requires <u>a</u>-prior pre-treatment, which is <u>achieved through a process known as</u> torrefaction, to enhance its quality as <u>thea</u> solid fuel. Torrefaction is a lignocellulosic biomass pre-treatment <u>process</u> at low temperatures between 473 <u>K</u> and 573 K under an inert atmosphere. It is a cheap technology but it <u>needsrequires</u> additional operating costs <u>due to the need</u> for thermal energy and nitrogen as a carrier gas. If torrefaction <u>cancould</u> be carried out in the presence of oxygen, <u>this willit would</u> reduce the operating expenses by <u>utilizing flue gas from the burners</u>⁴. Therefore, this study₇ aims to investigate the effects of oxygen <u>towardson the</u> torrefaction of EFB.

2. Experimental

The biomass residues used in this study were the consisted of empty fruit bunches (EFB) which were collected from Felcra Nasaruddin Ooil palm mill in Bota, Perak, Malaysia, Pprior to the torrefaction treatment, EFB were first chopped into smaller sizes and dried at 105 °C overnight forto remove the moisture removal. Then, EFB were was then grounded and further sieved to obtain a uniform particles size, ranging from 0.25 mm to 0.50 mm.

the experimental system where the torrefaction process was conducted consisteds of a vertical tubular reactor made of stainless steel with an internal diameter of 0.028 m and a length of 0.56 m, where the torrefaction process was conducted. The torrefaction reactor was connected to a condenser whichthat was immersed in ice cubes in order to collect the condensable gases (Figure 1). A 5-g sample of empty fruit bunches sample was placed in the centre of the reactor supported by with a glass wool and held with wire acting as its supporter and holder, respectively. Then, the system was flushed with torrefaction gas for 15 minutes with a flow rate of 100 mL/min. After the system was flusheding the system, the flow rate of torrefaction gas was reduced to 30 mL/min and the temperature of the reactor was raised from room temperature to the desired temperature using an electric furnace at a rate of 10 °C/min. Once the desired temperature was reached, the torrefaction temperature was maintained for 30 minutes. The torrefaction process produces solid, **Commented** [.1]: Please do not leave a space between the figure and the percentage sign.

Commented [.2]: There is no need to use 'approximately' here as 'roughly' is already being used to denote the lack of accuracy. Commented [.3]: Countries like 'Malaysia' should start with an upper-case letter.

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liquid and non-condensable products. <u>When cooled</u>, <u>T</u>the solid torrefied biomass was retrieved <u>later</u> from the reactor after it <u>has cooled down and beingwas</u> weighed. The condensed vapour phase was collect<u>ed</u> in a condenser and weighed. The solid yield is an important indicator <u>towhen</u> evaluatinge the severity of <u>the</u> torrefaction condition <u>towardsof</u> biomass. It can be calculated as <u>in</u> the following equation—1:

$$Y_m = \frac{m_{torrefied}}{m_{raw}} \times 100 \% (1)$$

where Y_m is the solid yield, $m_{torrefied}$ is the mass of torrefaction products and m_{raw} is the mass of torrefaction reactants. All weights reported were based on <u>a</u> dry basis.

The bulk densities of the untorrefied and torrefied biomass was were determined by measuring the mass of a known volume of EFB sample, which has been was placed in a measuring cylinder. Than the density was then measured based on the known volume and mass obtained.

The calorific values were determined using a bomb calorimeter, (model C2000 series manufactured by IKA Werke), The obtained calorific value obtained from the bomb calorimeter, which included the latent heat of the vapour, iswas produced from the sample.

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